

1 Article

2 Conjugate heat transfer characteristics in a highly 3 thermally loaded film cooling configuration with 4 TBC in syngas

5 Jing Ren^{1,*}, Xueying Li ^{1,†} and Hongde Jiang ^{1,†}

6 ¹ Institute of Gas Turbine, Department of Energy and Power Engineering, Tsinghua University;
7 renj@tsinghua.edu.cn

8 * Correspondence: ren@tsinghua.edu.cn; Tel.: +86-10-62796401

9 † These authors contributed equally to this work.

10

11 **Abstract:** The future power equipment tends to take hydrogen or middle/low heat-value syngas as
12 fuel for low emission. The heat transfer of film cooled turbine blade shall be influenced more by
13 radiation. Its characteristic of conjugate heat transfer is studied experimentally and numerically in
14 the paper by considering radiation heat transfer, multi-composition gas and TBC. The Weighted
15 Sum of Gray Gases spectral model and Discrete Transfer Model are utilized to solve the radiative
16 heat transfer in the multi-composition field, while validated against the experimental data for the
17 studied cases. It is shown that the plate temperature increases significantly when considering the
18 radiation and the temperature gradient of the film cooled plate becomes larger. It is also shown that
19 increasing percentage of steam in gas composition results in increased temperature on the film-
20 cooled plate. The normalized temperature of the film-cooled plate decreases about 0.02, as the total
21 percentage of steam in hot gas increases per 7%. As for the TBC effect, it can smooth out the the
22 temperature distribution and insulate the heat to a greater extent when the radiative heat transfer
23 becomes significant.

24

25 **Keywords:** film cooling; conjugate heat transfer; radiation; syngas; TBC

26

27 1. Introduction

28 The future advanced power generation cycles are supposed to utilize hydrogen or middle/low
29 heat-value syngas as fuel, aiming to realize Zero-Emission or Near-Zero Emission. In detail, the
30 thermal performance of turbines depends on moist gases composition. Furthermore, the radiative
31 heat transfer can be enhanced when the turbine inlet temperature grows. Also, the varied gas
32 composition due to fuel variation will impact the turbine heat transfer performance, since steam and
33 carbon dioxide are far more radiative than air or nitrogen diluted gas stream [1]. The thermal barrier
34 coating (TBC), as a semitransparent medium for radiation, is influenced by the gas compositions and
35 radiation at the same time. Therefore, it is important to predict temperature distribution of thermal
36 components accurately, especially considering radiative heat transfer.

37 The conjugate heat transfer method is widely adopted in the design of the high-thermal loaded
38 components of gas turbines. Bohn et al. [2-7] used the self-developed code and conducted
39 comprehensive studies on the conjugate heat transfer performance of turbomachinery. Mansour et al.
40 [8] investigated the effect of transition model on the accuracy of conjugate heat transfer simulation.
41 Heidmann [9] investigated the boundary element method (BEM) in simulating the three-dimensional
42 film-cooled turbine vane, and two materials with different thermal conductivity were considered.
43 The work of Hylton et al. [10-11] conducted detailed surface temperature measurements at the

44 midspan of the Mark II and the C3X vanes. The data of Hylton is widely used as benchmark data for
45 conjugate heat transfer simulations. Recently, Dees and Bogard et al. [12-14] conducted a series of
46 experiments of a turbine vane including adiabatic and conjugate heat transfer conditions.

47 Efforts focused on the effects of radiative heat transfer on the gas turbine have been widely
48 conducted. Kumar and Kale [15] conducted conjugate heat transfer simulation of a two-dimensional
49 blade by a FEM based numerical scheme. The computational results showed that the radiative heat
50 transfer was decreased if the TBC was included. He and Tan [16] simulated the radiative heat transfer
51 process in a three-dimensional engine vane adopting the discrete ordinates model. The results
52 indicated that the incident radiative heat fluxes increase from 188% to 212% as the inlet gas
53 temperature increase 29.9%. Zhang et al. [17] utilized a coupled fluid-thermal model to investigate
54 the conjugate heat transfer characteristics of 3D turbine blade by adopting P-1 radiation model. It was
55 shown that the blade surface temperature increased significantly and varied a lot when considering
56 the inlet radiation. Akwaboia et al. [18] investigated the combined effects of radiation heat transfer
57 and heat conduction in the semitransparent TBCs. Their results showed that the temperature of the
58 metal substrate with TBC exceeded over about 40 K than that without radiation. Mazzotta et al. [19]
59 investigated the temperature distribution on a E3 airfoil with the turbine inlet temperature exceeding
60 1700°C. They considered varied gas compositions, with employing P-1 model for solving radiative
61 heat transfer equation. It was shown that the contribution of radiation on the total surface heat flux
62 was up to 5.7%.

63 The effect of the hot gas compositions on the turbine heat transfer performance was also
64 investigated in recent studies. S. Na et al. [20] studied the effect of varying hot gas composition on
65 the temperature distribution of flat plate. The results showed that varying hot gas composition has a
66 significant influence on the maximum temperature distribution of a film-cooled flat plate. Moliere
67 et.al [21] reported that increasing 1% radiative heat transfer resulted in a temperature increment of
68 2.3K on the airfoil surface. As for the TBC, Feuerstein [22] reviewed the effect of TBC materials on the
69 thermal performance of turbine airfoil. Bohn et al. and Davidson et al. [23, 24] investigated the effect
70 of TBC on the temperature distribution of gas turbine.

71 In the present study, a high temperature test rig was built up to investigate the conjugate heat
72 transfer performance of a flat plate with a row of film cooling holes, considering the combination of
73 conduction, convection and radiation. The hot gas is about 800°C while the coolant air about 400°C.
74 The present study reviews the thermal performance considering the radiation heat transfer, hot gas
75 composition, and TBC. The hot gas compositions are the combustion products of liquefied petroleum
76 gas (LPG), natural gas (NG), syngas (syn), hydrogen (H₂) and oxy-fuel gas (oxy). Both experimental
77 and numerical methods are employed to understand the interaction among conjugate heat transfer,
78 gas compositions and TBC.

79 2. Experimental Apparatus

80 Figure 1 shows the highly thermal-loaded film cooling test rig, which is built up in Tsinghua
81 University, China. The test rig is composed of five main parts: the hot main gas inlet system, the
82 coolant air supply system, the film plate test section, the exhaust section and the measurement
83 system. The five parts will be described in detail in the following sections.



Figure 1. Highly thermally loaded film cooling test rig

2.1. Hot Gas And Coolant Air Supply Systems

Figure 2 shows the schematic representation of the test rig. The hot main gas system includes fuel injection section and burner section and produce hot gas with temperature of 800 °C. The fuel is mixed with air and is ignited in a 380Mcal/h burner. The fuel is liquefied Petroleum Gas (LPG) and has a flow rate from 15 to 30 kg/h, regulating the burner output power at a range of 200~400Mcal/h. The combustion products leave the burner with a temperature of about 2000 °C and entered the diluting section. The hot gas is mixed with the diluting air and the sprayed water, supplied by the top blower and the water supply system respectively. The resulting hot multi-composition gas is 800 °C.

The second system is the water supply system, which is used to adjust the hot gas composition with water. Eight spraying nozzles are spaced equally around the diluting section, delivering the diluting water into the section. The water flow rate is adjusted by the water supply pressure. The secondary coolant air is generated by a second blower and then is heated by an electric heat exchanger. The resulting air temperature is about 400 °C. Both the mainstream and coolant air channels are covered with heat-insulated layers.

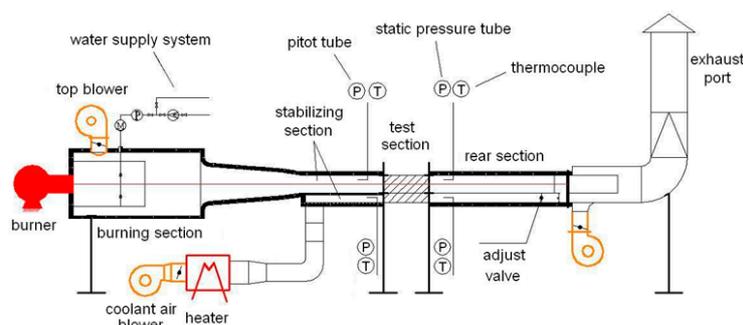


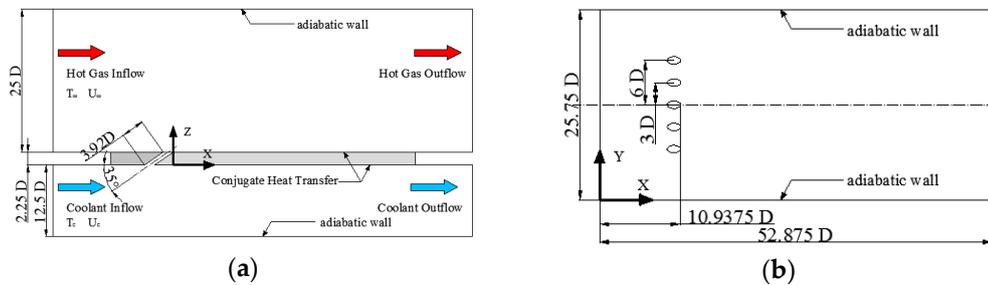
Figure 2. Schematic representation of test rig

2.2. Test Section

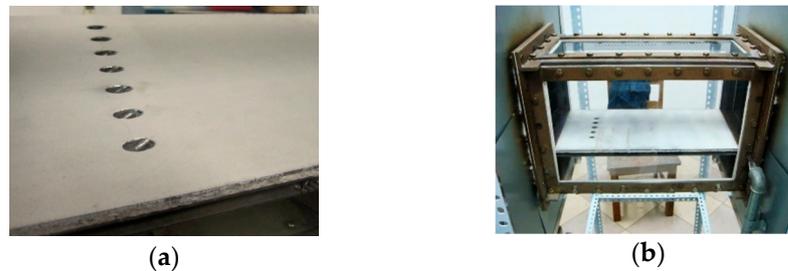
The test section is composed of internal cooling side and film cooling side, which is a typical cooling section of a turbine airfoil. The film cooling side hot gas temperature is 800 °C and the internal cooling side air temperature is 400 °C. The film cooling side and the internal cooling side are separated by a nickel-based superalloy flat plate with a thickness of 18 mm, as shown in Fig. 3. A row of seven film holes are arranged on the nickel-based superalloy plate, with a hole diameter of 8 mm. The film hole pitch is 3D, the hole inclination angle is 35°, and the length of the hole is $L=3.92 D$. The distance between the trailing edge of the holes and the inlet of the plate is 11D, while between the trailing edge of the holes and the outlet of the plate is 42D. On the top surface of the superalloy plate, TBC is sprayed by utilizing APS (Air Plasma Spraying) method, which is shown in Fig. 4. The top

114 coat is 0.5mm thick and the bond coat is 0.2mm thick. The thermal conductivities of the superalloy
 115 plate and TBC are 20W/mK and 2W/mK, respectively. But they will change with temperature.

116 The hot gas and the coolant air are at a speed of 15~20 m/s. An adjustable valve is installed in
 117 the cooling air channel, and by decreasing the flow area of the coolant air channel, the back pressure
 118 of the coolant air channel is higher than that of the hot gas channel. The blowing ratios are varied by
 119 adjusting the coolant and mainstream pressure difference.



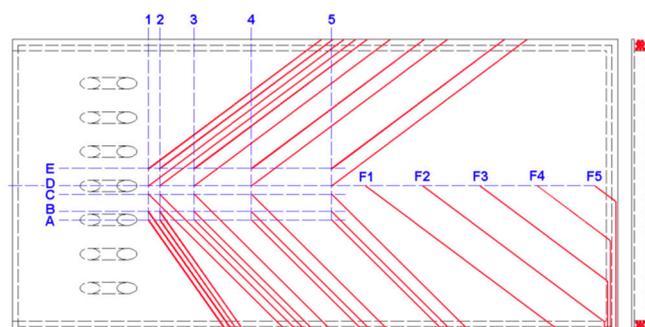
120 **Figure 3.** Schematic drawing of the test section, (a) Front view of the test section; (b) Top view of the film
 121 cooled plate



122 **Figure 4.** Superalloy plate and test section, (a) Photo of the superalloy plate; (b) Photo of the test section

123 2.3. Measurement System

124 The measuring system includes the pitot tubes, the static pressure tubes, the thermocouples, and
 125 the chromatographic analyzer. Four thermocouple are implemented at the center point of inlet and
 126 outlet of mainstream channel and coolant channel, measuring the temperatures of the inflow and the
 127 outflow, as shown in Fig.2. The inflow velocity is obtained by two pitot tubes that are installed in the
 128 center of each channel at the inlet of the test section. The back pressures of the channels are acquired
 129 by the static pressure tubes located at the outlet of the test section. In the downstream area of the
 130 centered film cooling hole, 90 thermocouples are installed on both top surface, bottom surface and
 131 middle of the plate, as shown in Fig. 5 and Table 1. The gas collecting tube locates at the stabilizing
 132 section of the hot main gas channel. The composition of the hot gas is determined by the
 133 chromatographic analyzer from the gas sample collected.



134

135

Figure 5. Schematic drawing of thermocouple positions on the plate

136

Table 1. Positions of the thermocouples.

Thermal couple positions	1	2	3	4	5	F1	F2	F3	F4	F5
Distance from the trailing edge of the hole to the thermocouple	1 D	2 D	5 D	10 D	17 D	20 D	25 D	30 D	35 D	40 D

137

138 The measurement uncertainty of the thermocouple is 0.3% and of chromatographic analyzer is
 139 2.2%. The uncertainty of the test system for temperature measurement is about 2.3%. The correction
 140 factors of the pitot tubes and the static tubes are calibrated to be unity.

141 3. Numerical Methodology

142 The numerical algorithm applied in the present study is conjugate heat transfer method, which
 143 consider the thermal conduction, convection and radiation in the computation. Commercial software
 144 ANSYS CFX 12.1 is adopted for all the numerical studies. The radiation heat transfer equation is
 145 solved by utilizing the discrete transfer radiation model (DTM). The absorption coefficient of the gas
 146 is determined by the weighted sum of gray gases (WSGG) spectral model. The numerical method is
 147 validated by comparing computational results with the experimental data.

148 3.1. Test Section Radiation Model

149 In the present study, the discrete transfer model (DTM) is employed due to the optical thickness
 150 of the radiation is less than unity. The DTM depends upon the discretization of the equation of
 151 transfer along multiple rays leaving from the bounding surfaces. The radiation transport governing
 152 equation is expressed as follows:

$$153 \frac{dI_v(\vec{r}, \vec{s})}{ds} = -(K_{av} + K_{sv})I_v(\vec{r}, \vec{s}) + K_{av}I_{bv}(v, T) + \frac{K_{sv}}{4\pi} \int_{4\pi} I_v(\vec{r}, \vec{s}') d\Omega' + S \quad (1)$$

154 The DTM is based on the assumption that operating system is homogeneous. the intensity Iv is
 155 solved along the rays leaving from the boundaries in the following form:

$$156 I_v(\vec{r}, \vec{s}) = I_{vo} \exp(-(K_{av} + K_{sv})s) + I_{bv}(1 - \exp(-K_{av}s)) + K_{sv}\bar{I}_v \quad (2)$$

157 The homogeneity assumption is maintained to extend the solution to the entire domain. It is
 158 then integrated over a solid angle to obtain the spectral incident radiation and the radiative heat flux
 159 at discrete points.

160 3.2. Spectral Model

161 For computation of the gas radiation properties, the weighted sum of gray gases (WSGG) model
 162 is the most widely model option, which is a compromise between the complete model that considers
 163 the particular absorption bands [25] and the oversimplified gray gas model. The WSGG model is
 164 combined with the DTM to obtain the emissivity of H₂O and CO₂. In the WSGG model, the gas
 165 emissivity is a weighted sum of gray gas emissivity in the following expression:

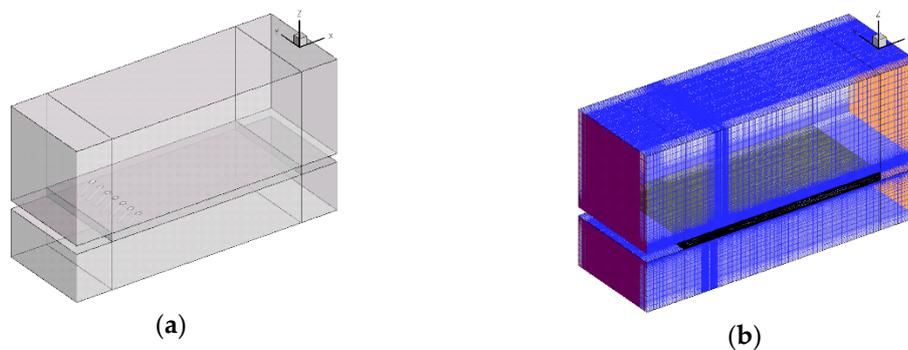
$$166 \varepsilon = \sum_{j=0}^{N_g} a_j(T) [1 - \exp(-k_j s)] \quad (3)$$

167 where a_j and k_j are the weighting factor and the absorption coefficient for the j^{th} gray gas component,
 168 respectively. The s is the path length. There exists a constraint that the sum of coefficients a_j is equal
 169 to unity when calculating coefficients of a_j and k_j . The transparent regions of the spectrum are

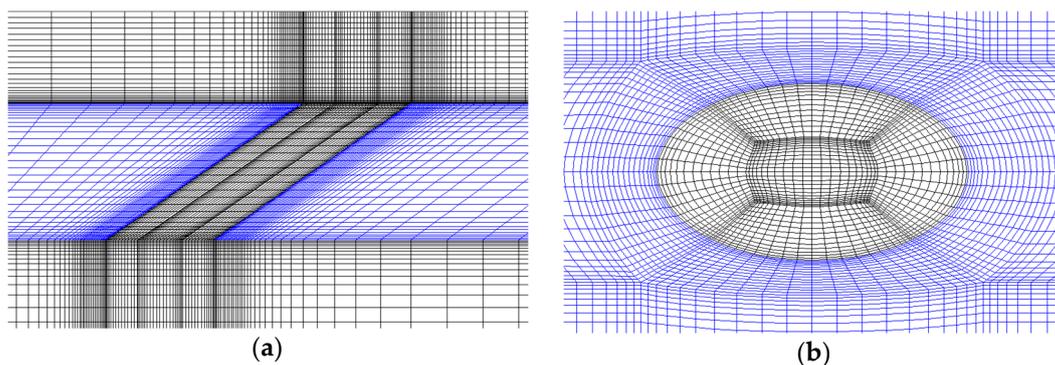
170 indicated by the term $j = 0$. The coefficients (a_j and k_j) from references [26] and [27] are used in the
 171 study. The partial pressure ratios of H₂O and CO₂ (H₂O/CO₂) are 1 and 2 when the number of gray
 172 gases is 3 [26]. The coefficients are applied when gas temperature falls within the range of 600 to 2000
 173 K and the partial pressure-path length products are from 0.001 to 10.0 atm-m. The property values
 174 are adequately predicted and are designated as "Smith 4GG". The partial pressure ratios of H₂O and
 175 CO₂ (H₂O/CO₂) are 2 and 3 when the number of gray gases is 4 [27]. The model is designated as
 176 "Perry 5GG". A more detailed description of the model can be found in reference [28].

177 3.3. Computational Geometry and Domain

178 The computational geometry is similar to the test section, including hole geometries, coolant and
 179 mainstream supply system. The inlet and outlet sections are extended by 10D to generate stable flow
 180 boundary conditions as shown in Fig. 6. Figure 7 shows the multi-block structured mesh, which is
 181 refined near the film-cooling holes and near-wall regions. More than 10 points are implemented in
 182 the boundary layer to achieve y^+ less than unity. The total element amount of the mesh is about 7.94
 183 million. A grid refinement is conducted to generate a mesh with 12.20 million cells and check mesh
 184 independent study. The results show that the two sets of meshes behave quite similar, and hence the
 185 mesh with 7.94 million cells is adopted in the present simulations.



186 **Figure6.** Computational domain and the structured mesh (a) Computational domain; (b) Multi-block
 187 structured mesh.



188 **Figure7.** Details of the structured mesh, (a) refined mesh near the plate; (b) refined mesh around the film
 189 cooling hole.

190 3.4. Turbulence model and Boundary Conditions

191 The SST $k-\omega$ turbulence model of Menter is adopted in the steady RANS simulations. The $k-\omega$
 192 model is used in near wall regions and the $k-\epsilon$ model is switched on in mainstream region. The mass
 193 flow rate boundary condition is applied at the inlet section and steady pressure is applied at the outlet
 194 section. The top and bottom surfaces of the test plate are heat transfer interface between fluid and
 195 solid domain. The other walls around the fluid domain are temperature wall, and the temperatures
 196 are measured by thermocouples.

197 3.5. Material Parameters

198 In the present simulations, the specific heat and thermal conductivity of the nickel-based
199 superalloy vary with temperature and are provided in reference [29]. The emissivity of the Nickel-
200 based superalloy plate is set as 0.79 [30]. Ideal gas assumption is used in the simulations, where the
201 specific heat capacity of the gas is calculated by the NASA format polynomials. The gas transport
202 properties are obtained from the REFPROP program that is an acronym for reference fluid properties
203 [31].

204 3.6. Validation of the numerical algorithm

205 Based on the configuration of the test rig, three gas composition cases are studied to validate the
206 numerical algorithm. The gas compositions of each case are listed in Table 2. Varying the steam
207 humidity of hot gas can change the gas composition. Other boundary conditions of the three
208 experimental cases keep the constant, which is shown in Table 3.

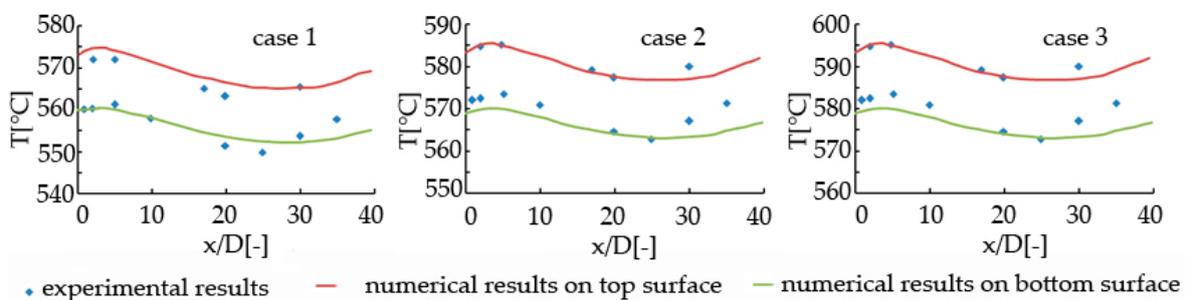
209 **Table 2.** The experimental hot gas compositions

Compositions (Volume %)	Case 1	Case 2	Case 3
H ₂ O	11.86	22.34	26.15
CO ₂	5.28	7.14	7.80
O ₂	10.26	5.55	3.87
N ₂	72.60	64.97	62.18

210 **Table 3.** Experimental boundary conditions

Parameters	Mainstream	Coolant Flow
Inlet Temperature [°C]	800	389
Inlet Mass Flow Rate [kg/s]	0.217	0.140
Outlet Pressure [pa]	101407	101428

211 Figure 8 shows the experimental and numerical centerline temperature distribution along the
212 centerline on the top and bottom plate surfaces. The red line indicates temperature distribution on
213 the top surface, and the green line indicates the temperature distribution on the bottom surface. It is
214 shown that the numerical results agree well with the experimental results for three cases. Therefore,
215 it is concluded that the DTM and WSGG model are adequately accurate for the present cases.



217 **Figure 8.** Centerline temperature distribution on the top and bottom surfaces of the film cooled plate

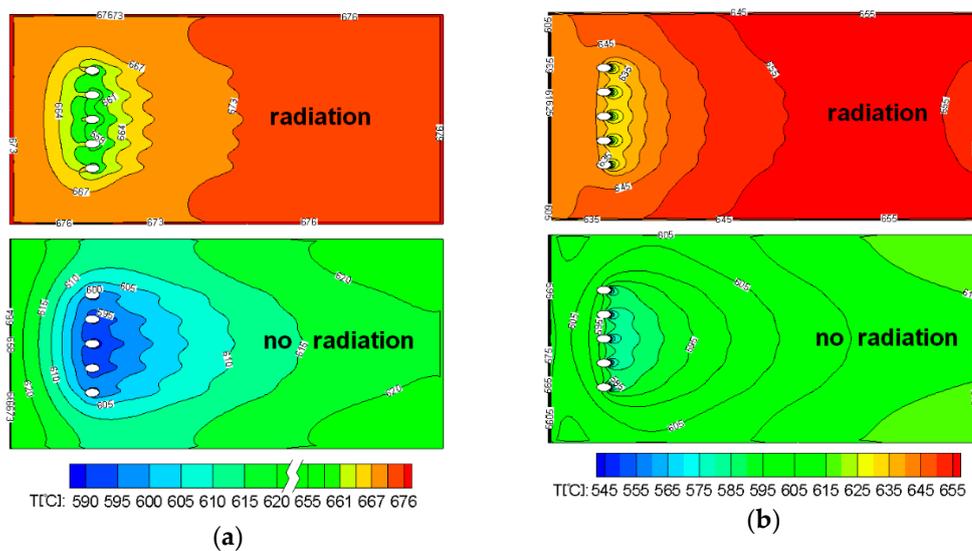
218 4. Results and Discussion

219 4.1. Effect of Radiative Heat Transfer

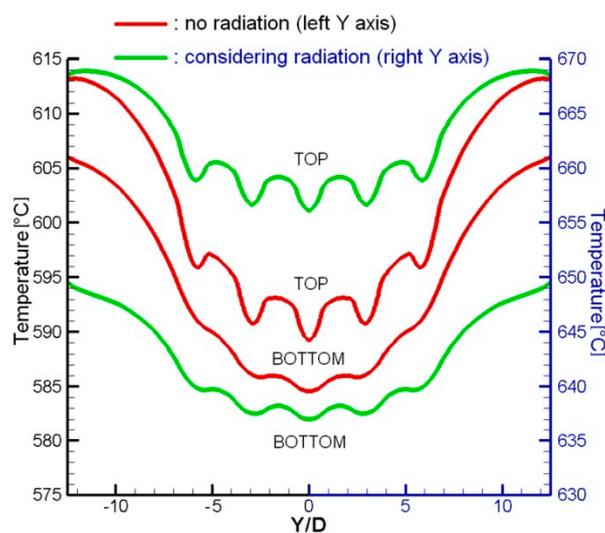
220 A pair of numerical cases with/without radiation are carried on to study the effect of radiative
 221 heat transfer based on the validated algorithm. The numerical study corresponds to a selected test
 222 cases with a mass fraction of H₂O is 7.92. The detailed information of the selected test case could be
 223 found in the Ref. 32.

224 The temperature distributions on the top and bottom sides of film plate resulted from the
 225 numerical study are showed in Fig. 9 for both with/without radiation cases. It is noted that the
 226 temperature level is significantly increased after considering the radiation for both the upper and
 227 bottom surfaces. Also the temperature patterns are changed if the plate is subjected to radiation,
 228 especially on the top surface where film cooling occurs.

229 Continually, the spanwise averaged temperature profiles on the top plate surface in both cases
 230 are shown in Fig. 10. It is noted that, on both top and bottom surfaces near the film cooling hole,
 231 the temperature profile in the spanwise direction becomes smoother when considering the radiation.
 232 This means radiation decreases the temperature gradient in the spanwise direction.



233 **Figure9.** Temperature distribution with/without radiation (a) on the top surface; (b) on the bottom
 234 surface.



235
 236 **Figure10.** Spanwise averaged temperature profile on the top plate surface, X/D=1

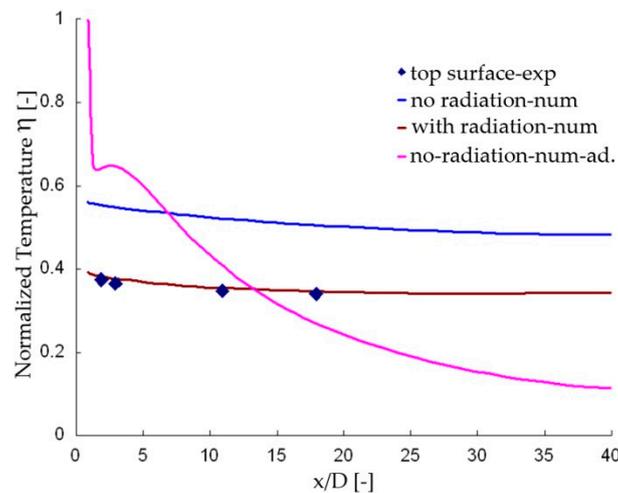
237 To further quantify the effect of radiative heat transfer, a normalized temperature η is defined
 238 by the following expression:

239

$$\eta = \frac{(T_w - T_c)}{T_g - T_c} \quad (4)$$

240 where T_g , T_c , T_w are the temperatures of the hot gas, the coolant air and the top surface wall. The
 241 normalized temperature is similar to the film cooling effectiveness when the plate surface is adiabatic.

242 Figure 11 shows line plots of η along the centerline of the plate top surface, an adiabatic case is
 243 employed as the basic. Compares with the case with no radiation, the normalized temperature of the
 244 case with radiation is about 0.2 lower, and even is lower than the adiabatic effectiveness before $x =$
 245 $13D$, the high cooling effectiveness near the holes almost disappears. That is to say, the film cooling
 246 effect is weakened by radiation while it further smears out the temperature gradient. In real engine
 247 conditions, hot main gas temperature will be higher than 1200°C (much higher than the condition of
 248 the test rig), and leads to high surface temperature and high local temperature gradient, which will
 249 result in significant thermal-mechanical load. The radiation enhances the temperature increasing, but
 250 weakens the temperature gradient.



251

252

Figure 11. Normalized temperature along the centerline of the top plate surface

253 4.2. Effect of Hot Gas Composition

254 The effect of the hot gas composition on the film cooling system is investigated by varying five
 255 different kinds of fuel. The hot gas compositions for each fuel are listed in Tab. 4.

256

Table 4. Hot gas compositions in the numerical study¹

Type of Fuel	Mole fraction [%]				
	CO ₂	H ₂ O	N ₂	Ar	O ₂
LPG	4.44	12.34	71.50	0.00	11.72
NG	5.66	11.08	74.66	0.00	8.60
Syn	9.27	8.50	72.80	0.80	8.63
H ₂	1.40	17.30	72.20	0.90	8.20
Oxy	16.00	82.00	1.10	0.80	0.10

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¹ The hot gas are the products of combustion of liquid petroleum gas (LPG), natural gas (NG), syngas (syn), hydrogen gas (H₂), and oxy-fuel gas (oxy).

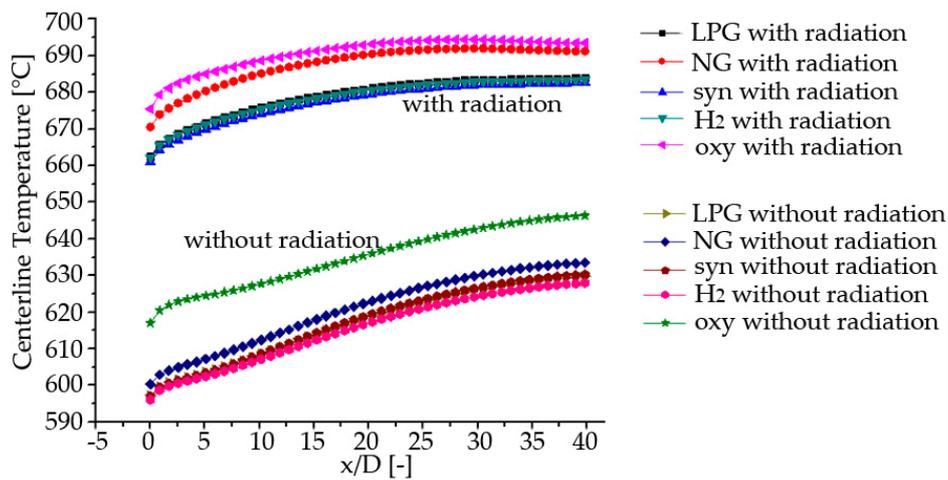
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Figure 12 shows the temperature distribution along the centerline of the top surface for five different fuels, with and without considering the radiation. Without considering radiative heat transfer, the temperature distributions are similar for five different fuel cases. Nitrogen is the major

263 composition of the hot gases and its mole fraction is more than 70%, while steam is the major
 264 composition of the combustion product of oxy and its mole fraction is 82%. Therefore, it is observed
 265 that the temperature distribution for the combustion product of oxy is about 15 °C higher than the
 266 other four gases. When considering the radiative heat transfer, a temperature rise about 50 °C is
 267 observed. A great temperature rise occurs for the combustion product of the natural gas has, which
 268 leads to a quite close temperature distribution to that of the combustion product of the oxy-fuel gas.
 269



270

271 **Figure 12** Temperature distribution along the centerline of the plate with/without radiation

272 4.3. Effect of Thermal Barrier Coating (TBC)

273 The effect of thermal barrier coating on the heat transfer performance is experimentally
 274 investigated. three different hot gas compositions are investigated after spraying TBC on the top
 275 surface of the plate. Table 5 shows the different gas compositions with and without TBC.

276

Table 5. Hot gas compositions in experiments with/without TBC.

Compositions (Volume %)	Case 1 Without TBC	Case 1 With TBC	Case 2 Without TBC	Case 2 With TBC	Case 3 Without TBC	Case 3 With TBC
H ₂ O	11.86	11.27	22.34	22.66	26.15	25.01
CO ₂	5.28	6.13	7.14	6.23	7.80	8.65
O ₂	10.26	10.07	5.55	5.25	3.87	4.94
N ₂	72.60	72.53	64.97	65.86	62.18	61.40

277

278 Figure 13 shows the experimental centerline temperature results on the top and bottom sides of
 279 the film plate. It is observed that the temperature patterns show a quite similar trend with and
 280 without TBC. In particular, the temperature is at high value the inlet, then decreases as x/D increases,
 281 and increases at the downstream region.

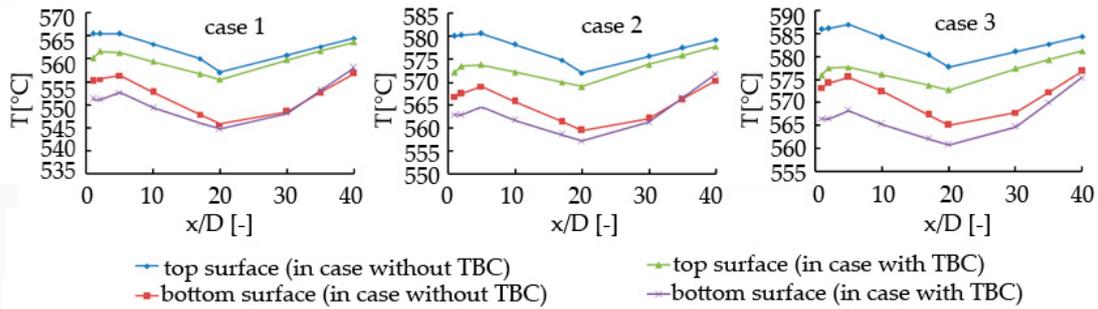
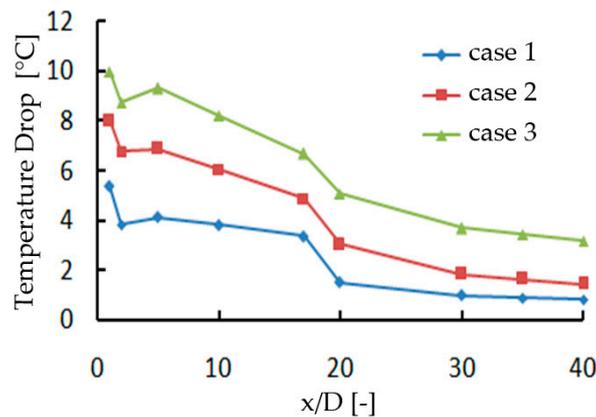


Figure13. Temperature along the centerline of the test plate surface

282
283

284 The temperature drops inside TBC are shown in Fig.14, which is derived from the results of three
285 pair of cases. It is clear that, in case 3, a higher percentage of steam results in a greater temperature
286 drop. By observing the temperature drop distribution with x/D , it is observed that the temperature
287 drop reaches maximum value at the entrance section, and decrease as x/D increases. This is associated
288 with the radiation distribution feature, i.e., a larger humidity causes a stronger radiation. Therefore,
289 the radiation is strongest at the entrance section, and grows weaker as x/D increases, which indicates
290 the temperature drop by TBC is higher when radiation effect is stronger.



291

Figure14. Temperature decrease inside TBC along the centerline of the test plate top surface

293 Therefore, it is concluded that the heat insulation effect of TBC is grows more obvious when the
294 radiation effect is significant. This is caused by the radiation property differences between TBC and
295 nickel-based alloy. However, when TBC is coated, over 50% of the radiation heat transfer is reflected
296 by TBC, which means TBC absorbs less radiation heat than superalloy and protects the metal
297 substrate. Another advantage of TBC is that it smooths the temperature distribution and decreases
298 the temperature gradient to some extent. More discussion can be found in [33].

299 5. Conclusion

300 Gas turbine film cooling system shows complicated flow and heat transfer characteristics due to
301 the interaction of heat conduction, heat convection and radiation heat transfer. In the present study,
302 the conjugate heat transfer characteristics of a film cooling system are experimentally and
303 numerically analyzed. The topics include the radiation heat transfer, multi-composition gas and TBC.
304 In solving the radiative heat transfer in the multi-composition field, the Discrete Transfer Model
305 (DTM) and the Weighted Sum of Gray Gases (WSGG) spectral model are employed and validated.

306 The results show that the surface temperature increase significantly and the temperature
307 gradient through the plate becomes much larger when the radiation is considered. It is also observed
308 that a higher percentage of steam in gas composition results in a higher temperature (lower
309 normalized temperature) on the film-cooled plate. In particular, the normalized temperature on the
310 film-cooled plate decrease about 0.02 as the percentage of steam in hot gas increases per 7%.

311 Furthermore, the heat insulation effect of TBC grows more obvious when the radiation heat transfer
 312 is stronger. Also observed is that TBC smooths the temperature distribution and thus decreases the
 313 temperature gradient to some extent.

314 Nomenclature

a	Emission weighting factor	[-]
D	Diameter of the hole	[m]
I_{bv}	Spectral black body emission intensity	[Wm ⁻³ sr ⁻¹]
I_v	Spectral radiation intensity	[Wm ⁻³ sr ⁻¹]
I_{v0}	Radiation Intensity leaving the boundary	[Wm ⁻³ sr ⁻¹]
K_{av}	Spectral absorption coefficient	[m ⁻¹]
K_{sv}	Spectral scattering coefficient	[m ⁻¹]
k	Absorption coefficient	[m ⁻¹]
L	Length of the hole	[m]
N_g	Number of gray gases	[-]
\vec{r}	Position vector	[m]
S	Radiation intensity source term	[Wm ⁻⁴ sr ⁻¹]
s	Path length	[m]
\vec{s}	Direction vector	[m]
T	Temperature	[K]
X, Y, Z	Cartesian coordinates	[m]
y^+	Dimensionless wall distance	[-]

315 Greeks

ε	Total gas emissivity	[-]
η	Normalized temperature	[-]
ν	Frequency	[s ⁻¹]
Ω	Solid angle	[sr]

316 Subscripts

c	Coolant flow
g	Gas
j	Index
w	Wall

317 Acronyms

DTM	Discrete transfer model
RTE	Radiation transport equation
WSGG	Weighted sum of gray gases

318

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