STREAMLINE'S SHAPE THEORY

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1   **Abstract:**   This article attempts to formulate a mathematical model for a potential explanation regarding
2   the unavoidable impact of a rigid body's peculiar shape on the seamless flow over it. The solid body
3   completely immersed in a Newtonian fluid and respectively has a relative open circuit flow on it will
4   typically experience various observable phenomena like flow separation, flow transition, down-wash,
5   stalling at the higher angle of attack, stalling velocity and how cambered airfoil can typically generate lift at
6   a zero incidence angle. This article respectively represents an understanding of the laminar flow over a rigid
7   body's external surface with due respect to its distinctive shape and size. This working paper formulates a
8   more realistic and simplified mathematical model for open circuit laminar flow over a body, based on the
9   historical data of aerodynamics and theoretical mechanics. This is intended to properly estimate forces
10 on the continuous surface of the body in a laminar flow, to properly explain, understand and predict
11 mentioned phenomena. Most of all the mechanism of streamline formation and its deformation with due
12 regards to flow, shape and size of the body in an open-circuit laminar are formulated mathematically to
13 enhance better design theory which can reduce experimentation while designing a streamlined body.

14 **Keywords:** General fluid mechanics ; Mathematical Model ; Streamline ;Flow–structure interactions ;
15 Topological fluid dynamics

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16 ## 1. Introduction

Fluid dynamics remain a peculiar field of study as the fluid particles are very miniature in their dimensions along with negligible masses and the solid bodies interacting with them have a considerable mass and size. Therefore, it is often ambiguous to identify which particular theories among classical mechanics, or quantum mechanics are applicable for a given model of a fluid dynamic system. In the context of Philosophy and History of the fluid dynamics, the approach of classical mechanics has been observed to be not very effective in describing and predicting an open-circuit flow.The popular Navier–Stokes equation is based on Isaac Newton's second law to fluid motion, together with the assumption that the stress in the fluid is the sum of a diffusing viscous term (proportional to the gradient of velocity) and a pressure term hence describing viscous flow. Though Navier–Stokes equation has a wide range of practical applications, it has not yet been proven whether solutions always exist in three dimensions and if they do exist, whether they are smooth – i.e. they are infinitely differentiable at all points in the domain. Moreover, Navier– Stokes equations are not conservation equations, but rather a dissipation system, in the sense that they cannot be put into the quasi-linear homogeneous form and Newton's second law is an approximation that is increasingly worse at high speeds because of relativistic effects[11]. Mathematically, Newton's 2nd law can be written as:

$$\vec{F} = m\frac{d\vec{v}}{dt} = ma \tag{1}$$

But the above statement seems to disagree with the historical observation by nearly 50 percent and what happened to the other 50 percent of force and how to contemplate that with appropriate assumptions.Consider a dimensional analysis for Newton's second law with the product of dynamic pressure and area. Thus, the product of pressure and area shall be equal to the rate of change of momentum of a body[11].

$$\vec{F} = \frac{1}{2}\rho\vec{v}^2 \times A = \frac{1}{2}\frac{m}{l^3}\frac{l^2}{t^2} \times l^2 = \frac{1}{2}ma \tag{2}$$

17   Here, $\vec{F}$ is sum of several forces such as inertial force, gravitational force, capillary force, compressibility or
18 elastic Force, internal force and pressure force. The flow of a fluid in practice does not involve all the forces
19 simultaneously.

20   Moreover, many theories under circulation increase ambiguity towards the understanding of various
21 phenomena such as flow separation, stalling of the body, transition of flow from laminar to turbulent. All
22 these theories define only a few specific aspects of the flow and each of them tentatively identifies with all the
23 possible effects. Most of all, theoretical literature that can explain few phenomena such as the mechanisms
24 of streamline formation and shock waves formation is observed to be and unavailable.

25   Fluid dynamics concerning to a rigid body which is relatively moving in a Newtonian fluid more like an
26 aircraft or submarine will undergo various phenomena. Depending on the various factors such as nature
27 of the flowing fluid and nature of the fluid flow the forces acting efficiently on the body can be expressed
28 as functions of fluid density(ρ) , dynamic viscosity of the fluid(μ) , free stream velocity($\vec{v_\infty}$) , effective
29 Area(A)[8]. But when it comes to the shape like thickness, length, the degree of curvature of the body and
30 its relative effect on the flow, they are often determined by employing the experimental methods[10].

According to Newton's "Philosophiæ Naturalis Principia Mathematica-Book II", the resultant force on a
body is a function of the fluid nature, flow nature, shape and size of the body interacting with fluid [6].

$$\vec{F} = \{\rho, \vec{v}, c_{fluid}, \mu, A, l\} \tag{3}$$

$$\vec{F} = \frac{1}{2}\rho_\infty \vec{v}_\infty^2 A_{ref} C_F \tag{4}$$

Equations (3) and (4) gives resultant force on the body which can also be given as a function of
similarity parameters like Mach number(M) and Reynold's number(Re)[4][7]. Here, equation (4) gives
the resultant force on the body due to the fluid flow over it as a function of flow parameters and area only.
Conventionally the resultant force is an aggregate effect of shear stress distribution and dynamic pressure of
the fluid over the body[4][7]. But these do not give an explanation why and how the shape is affecting the
flow. Often, the vertical component of resultant force and horizontal component of resultant force namely
Lift(L) and Drag(D) are traditionally written as shown in (5) and (6)[10][7].

$$\vec{F_y} = \vec{F}sin(\alpha) = \frac{1}{2}\rho_\infty \vec{v}_\infty^2 A_{ref} C_L \tag{5}$$

$$\vec{F_x} = \vec{F}cos(\alpha) = \frac{1}{2}\rho_\infty \vec{v}_\infty^2 A_{ref} C_D \tag{6}$$

31

32   In these equations, the force due to shear stress is ignored, and equations show forces as a product of free
33 stream dynamic pressure(q_∞) and a reference area(A_{ref}). So, there is always a deviation in calculated results
34 with respect to the actual magnitude of the force on the body. Thus, coefficients of forces (dimensionless
35 parameters) and reference area are considered rather than actual parameters. Therefore, there is always a
36 need for experimental methods to evaluate estimated values and to correct them. The corrections obtained
37 from experiments have to be substituted in the equation to obtain near exact calculations[10].

38   From these, we can undoubtedly understand that not just shape is ignored in extant conventional
39 formulae but the appropriate size of the body is not absolutely considered. The NACA reports regarding
40 camber, chord, and thickness of airfoil is another excellent example to show that not all aspects regarding
41 shape and size are not adequately considered in mathematical models and were evaluated using trail & error
42 methods. Notably, there is a lack of proper theoretical explanation and a mathematical model regarding
43 how shape affects the continuous flow and so on.

44   However, solid body interacting with fluid will have negligible effects due to fluid interaction at low
45 speeds. A mathematical model in terms of classical mechanics is more lucid, yet it has its a limitation
46 when continuum effects occur such boundary layers, ionization (mass or energy dissipation) and most
47 importantly classical mechanics studies a system within time intervals. For any continuum effect trajectories

and forces alone don't play a key role in describing and predicting the system. A fluid dynamic system needs a space-time domain to understand and study the system properly.

Thus, there is a definite necessity for the theoretical fluid dynamics to bridge the gap between classical mechanics and quantum mechanics. Most of all, it is necessary to integrate several partial theories into a single unified theory which can explain these phenomena clearly. At the same time, it shall support a mathematical model that can be useful to predict these phenomenon as-well[3].

In terms of classical mechanics, motion of a fluid particle is studied with due respect to the forces and trajectories[3]. Thus formation of streamline and it's mechanism is vital phenomenon that need to be considered. This will be helpful in order to predict the impact of the shape and size over the flow.

2. Theory

2.1. Fundamental assumptions

1. The working fluid is typically assumed to be Newtonian fluid.
2. Flow is assumed to be two dimensional, irrotational, laminar flow.
3. Stream-lines are formed due to dynamic pressure and shear stress distribution.

2.2. Postulates

1. Fluid particles move freely as their inter-molecular forces are very negligible as long as there is no external influence.
2. When an external solid body typically comes in direct contact with a flowing fluid, the fluid particles bombard at the surface of the body and loose their considerable momentum and kinetic energy[5]. The energy typically lost by a collided fluid particle is convected to surrounding fluid particles as momentum while retaining internal energy.
3. Internal energy is converted to thermal energy and dissipates to the body and flowing fluid in contact with the fluid particles at the point of collision.
4. Similarly, momentum is also transferred to the collided particles from surrounding fluid particles which receive energy to continue the motion of collided particles. So, there will be change in velocity say $\Delta \vec{v}$ and temperature ΔT. This happens as a process of fluid particles trying to achieve thermodynamic equilibrium.Thus, velocity boundary layer and thermal boundary layers are formed, whose characteristics are given by *Prandtl's Boundary Layer*.[1]
5. However, if the body has enough strength to resist continuous displacement or deformation, the Newtonian fluid will go under displacement or deformation instantly forming a stream line around the body's external surface. Under high speed fluid dynamics shock waves and ionization are observed where internal energy of fluid particles undergo changes forming radicals.
6. The energy lost by flowing fluid on the surface of the body acts as a mechanical load in the form of dynamic pressure normally to body's surface and resistance offered by the surface will be the tangential to fluid flow which results in shear stress distribution[4][7][5].
7. Since the fluid particles are spatially spaced the inter-molecular distance changes and leads to compressibility as they are subjected forces from neighboring fluid particles. Thus, fluids have compressibility under motion.For a given compression (a decrease in volume), the increase in pressure is proportional to the bulk modulus of elasticity E. These effects are continuum.

3. Conditions

Now let's assume a rigid body moving in a Newtonian fluid. From above statements the magnitude of the resultant force $|\vec{F}|$ on the body due to relative motion between the fluid and corresponding body can be written as shown in equation (7).

$$\vec{F} = \left(\frac{1}{2}\rho v^2\right)A + \left(\mu \frac{\partial v}{\partial y}\right)A \qquad (7)$$

The resultant force ($\vec{F}$) will have angle with respect to the free stream velocity vector ($\vec{v_\infty}$) or the direction of the free stream. But the induced angle depends not just on angle of attack (α) but also on the shape and

90 size of the body. So there exists an angle in between the free stream and resultant of the force which has
91 been commonly observed in asymmetric bodies. This means the resultant force on the body will not be
92 in the direction of the free stream ($\vec{F}$ and $\vec{v_\infty}$ are not co-linear). It will have an angle with respect to the
93 free-stream (θ) even when angle of attack is zero($\alpha = 0°$). The direction of the fluid particles changed with
94 respect to free-stream forming an angle which resulted in the resultant force to slightly incline at angle θ
95 with respect to free stream. This change is due to the shape of the body. Thus, the resolution of the resultant
96 force in horizontal and vertical components gives D or $\vec{F}_X$ and L or $\vec{F}_Y$ equation (8) and equation (9).

$$\vec{F}_x = \left(\frac{1}{2}\rho v^2 cos(\alpha + \theta)\right)A + \left(\mu \frac{\partial v}{\partial y} cos(\alpha + \theta)\right)A \tag{8}$$

$$\vec{F}_y = \left(\frac{1}{2}\rho v^2 sin(\alpha_\infty + \theta)\right)A + \left(\mu \frac{\partial v}{\partial y} sin(\alpha + \theta)\right)A \tag{9}$$

Here, θ in equations (8) and (9) is the angle between the resultant force due to fluid flow and free stream
velocity, due to the change in streamline of particles along its length or simply the shape the of a body[6].
So, as per circulation theory the particles must move around the body in a circle when they fail to circulate
they form vortexes.[4] But, in reality fluid particles won't move in a circular path around a body. They will
split as two streamline on the upper surface and lower surface of the body. Thus for a circulation around
a body $\Sigma\theta$ should be 0°. Which means the resultant force should have no angular deviation with respect
free stream velocity. Equations (10) and (11) shows integral form of this circulation condition. Here, in
equations (10) and (11) θ_{uo} and θ_{lo} are the deviation of resultant force at the particular point on upper
surface and lower surface of the flow respectively.

$$\oint_{LE}^{TE} \theta_{uo} = \oint_{LE}^{TE} \theta_{lo} = 0 \tag{10}$$

$$\oint_{LE}^{TE} \theta_{uo} + \oint_{LE}^{TE} \theta_{lo} = 0 \tag{11}$$

4. Calculations

98 So let's evaluate the above conditions. To study the impact of shape and size over fluid's flow, let's
consider two successive space domains $A_i \& A_{i+1}$ in the flow as shown in Figure 1[3].
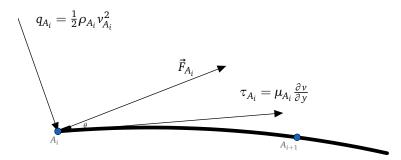
Figure 1. Illustration of the resultant force vector on successive space domains in a stream line

99

100 1. Consider a infinitesimally small area as shown in Figure 1. Figure 1 illustrates that the the force
101   vectors due to dynamic pressure and shear stress of any point A_i in streamline which will interact with
102   adjacent points A_{i+1}. On any given point A_i in the considered system where it has velocity $\vec{v}_i$. Upon
103   interaction with other corresponding particles in the streamline, the velocity will change to $\partial \vec{v}_i + \vec{v}_i$.
104 2. Thus there will be change in pressure normal to A_i which is $\partial q_{A_i} + q_{A_i}$. The force at A_i is normal
105   vector to area. But the corresponding Area A_{i+1} will have an additional force vector on it with certain
106   angle θ_i. As per the equations (8), (9) (10) and (11), the force vector is an integral function over
107   the stream lines. The resultant vector will be the sum of all the force vector which is ahead of the

108   considered infinitesimally small area A_i . For 2D flow it can be written as surface integral[8] So, $\vec{F}_{A_{iq}}$
109   can be written as the resultant fluid dynamic force at a infinitesimally small area due to the dynamic
110   pressure of subjected motion of fluid at A_i. $\vec{F}_{A_{iq}}$ is given quantitatively in equation (12).

$$\vec{F}_{A_{iq}} = \oiint_A \left(\frac{1}{2}\rho_{A_i} v_{A_i}^2 + \frac{1}{2}\rho_{A_{iq-1}} v_{A_{i-1}}^2 cos(\theta_{rxy}) \right) dA \tag{12}$$

111   Here dA is infinitesimally small area between the A_i and successive points. θ_{rxy} is the algebraic sum
112   of angles between resultant forces vectors $\vec{F}_{A_i}$ and $\vec{F}_{A_{i+1}}$ along the streamline over the surface.
113   3. Similarly, the effect of shear stress distribution of resultant force at A_i can be given as:

$$\vec{F}_{A_{i\tau}} = \oiint_A \left(\mu_{A_i} \frac{\partial v_i}{\partial y} + \mu_{A_{i-1}} \frac{\partial v_{i-1}}{\partial y} cos(\theta_{rxy}) \right) dA \tag{13}$$

114   Here, Equations (13) gives the effect of shear stress distribution over surface integral. As the second
115   components in the equations (12) to (13) are resultants of the succeeding elements and their effect is
116   dependent on the angle θ_{rxy} .
      4. Therefore, the resultant force at a infinitesimally small area A_i can be written as sum equations (12)
      and (13).

$$\vec{F}_{A_i} = \oiint_A \left(\frac{1}{2}\rho_{A_i} v_{A_i}^2 + \frac{1}{2}\rho_{A_{i-1}} v_{A_{i-1}}^2 cos(\theta_{rxy}) + \mu_{A_i} \frac{\partial v_{A_i}}{\partial y} + \mu_{A_{i-1}} \frac{\partial v_{A_{i-1}}}{\partial y} cos(\theta_{rxy}) \right) dA \tag{14}$$

117   Equation (14) gives the resultant force at any given point A_i, which is the sum of the products of
118   the area with shear stress and dynamic pressure[6][8][3]. The resultant force of the preceding fluid
119   particles can be resolved on the given point with an angle θ_r and the resultant will have an effect on
120   succeeding A_{i+1}.

Thus, equation (14) can be simplified as :

$$\vec{F}_{A_i} = \oiint_A \left(\frac{1}{2}\rho_{A_i} v_{A_i}^2 + \mu_{A_i} \frac{\partial v_{A_i}}{\partial y} + \vec{F}_{A_{i-1}} cos(\theta_{rxy}) \right) dA \tag{15}$$

$$\vec{F}_{A_i} = \oiint_A \left(\vec{F}_{A_i} + \vec{F}_{A_{i-1}} cos(\theta_{rxy}) \right) dA \tag{16}$$

The effect of $\vec{F}_{A_i}$ can be resolved in X-plane , Y-plane and Z-plane using trigonometric relations as
shown in equations (17) , (18) and (19). Here, $\theta_{r_x}, \theta_{r_y}$ and θ_{r_z} are the angles at which force at any
point A_i acts on surrounding fluid particles along X-axis, Y-axis and Z-axis respectively.

$$\Sigma_0^n(\theta_{r_x}) = \Sigma_o^n \sin^{-1} \frac{\sqrt{|\vec{F}_{A_{i_x}}|^2 - |\vec{V_i x}|}}{|\vec{V_{ix}}|} = 0 \tag{17}$$

$$\Sigma_0^n(\theta_{r_y}) = \Sigma_o^n \cos^{-1} \frac{|\vec{V_{iy}}|}{|\vec{F}_{A_{i_y}}|} = 0 \tag{18}$$

$$\Sigma_0^n(\theta_{r_z}) = \Sigma_o^n \sin^{-1} \frac{\sqrt{|\vec{F}_{A_{i_z}}|^2 - |\vec{V_i z}|}}{|\vec{V_{iz}}|} = \Sigma_o^n \cos^{-1} \frac{|\vec{V_{iz}}|}{|\vec{F}_{A_{i_z}}|} = 0 \tag{19}$$

121   Depending upon the direction of flow and it's magnitude the components of θ can be represented as
122   sin, cos components in the OX,OY planes. Here, $\vec{F}_{A_{i_x}}$ and $\vec{F}_{A_{i_y}}$ are resolved components of the resultant
123   force in X-plane, Y-plane respectively. where $\vec{V_{ix}} and \vec{V_{iy}}$ are velocity vectors of stream lines in X-plane
124   and Y-plane respectively.

125   Equations (17),(18) and (19) shows the trigonometric relations between local velocity vector, θ and force.
126   When the circulation conditions mentioned in equations (10) and (11) are applied, the algebraic sum of θ

127 along the stream line should be zero. Otherwise, streamline formation is disturbed leading to occurrence of
128 other phenomena such as vortex formation at trailing edge or down-wash.
129   So based on the above equations it can be explained that the formation of stream changes with the
130 degree of curvature of the body, its size, flow velocity, fluid density and dynamic viscosity of the fluid. As per
131 $3^r d$ and $4^t h$ postulates the energy is transferred or transformed between two time intervals i.e. energy or
132 momentum lost by collided fluid particles and energy received by collided fluid particles from its surrounding
133 fluid particles. So there can be two time intervals $t_1 - t_2$ and $t_2 - t_3$.

At a local area A_i the equation (16) can be written as:

$$\vec{F}_{A_i} = \int_{t_1}^{t_3} \left(\oiint_A \left(\vec{F}_{A_i} + \vec{F}_{A_{i-1}} cos(\theta_{rxy}) \right) dA \right) dt \qquad (20)$$

$$\vec{F}_{A_i} = \int_{t_1}^{t_2} \left(\oiint_A \left(\vec{F}_{A_i} + \vec{F}_{A_{i-1}} cos(\theta_{rxy}) \right) dA \right) dt + \int_{t_2}^{t_3} \left(\oiint_A \left(\vec{F}_{A_i} + \vec{F}_{A_{i-1}} cos(\theta_{rxy}) \right) dA \right) dt \qquad (21)$$

134 Equation (20) and (21) shows time integral of force at a local area (A) over the two successive events.
135 $t_1 - t_2$ is the time interval when fluid particle collide at the solid body's surface and loose their momentum
136 and time interval $t_2 - t_3$ is the period when collided particles receive momentum to continue their motion.
137 This is due to elasticity of the fluid and its tendency to attain thermodynamic equilibrium. Equation (20)
138 has both time integral and surface integral defining the force and angle at which the it is acting on the
139 corresponding fluid particle. The time integral defines the consecutive effects of the fluid particles motion
140 and surface integral corresponds to local changes on the surface. Where as the θ corresponds to the degree
141 of the curvature of the body which can be noted by the trigonometric relations shown in equations (17),
142 (18) and (19).

5. Discussions

143

5.1. Flow over a linear body

144

145   Consider a flat plate parallel to the free-stream with a smooth laminar flow as shown in Figure 2. In the
146 Figure 2 the flat plate 'f' has a viscous laminar flow which is indicated by dotted stream lines. The thickness
147 and style of lines indicate viscosity at that particular point. The free body diagram of 'f' shows force vectors
148 on upper surface and lower surface from leading edge to trailing edge. Here, $\vec{F}_{uo}$ is the resultant force
149 vector on upper surface and $\vec{F}_{lo}$ is the resultant force vector on lower surface at leading edge. $\vec{F}_{iu}$ and $\vec{F}_{il}$
150 are the resultant force at any given point in between leading edges and trailing edges respectively. θ_n is the
151 algebraic sum of all the respective angles of $\vec{F}_{A_i}$ over the flat plate i.e $\theta_{nu} + \theta_{nl} = \theta_n$. Here, $\Sigma_{0u}^{nu}\theta = \theta_{nu}$ and
$\Sigma_{0l}^{nl}\theta = \theta_{nl}$.
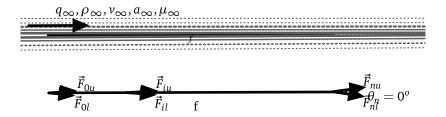
Figure 2. Laminar flow over a flat-plate

152
153   So, at stagnation point if the body with stands these forces then substantial phenomenon are observed:
154 Thus, the resultant force of the stagnant fluid particles will be at an angle with respect to free-stream velocity.
155 The resulting force from stagnation point, which is acting over the surrounding fluid particles makes them
156 to flow around the upper surface and lower surface of the body will have change in their $\theta_i u$ and $\theta_i l$ and
157 magnitude $\vec{F}_{iu}$ and $\vec{F}_{il}$. As the change in momentum simultaneously effects the viscosity and thus change

158 in the velocity vectors of fluid particles moving on the upper surface and lower surface will continuously
159 have a increment in the angle θ_i and the magnitude of the resultant force $|\vec{F}_i|$ till the trailing edge. If the
160 sum of θ_{nu} & θ_{nl} is equal to 0°.[6] Then fluid particles flow in same direction as free-stream as long as the
161 magnitude of $\vec{F}_n$ is not too high to deviate them from channeled stream line. Thus at low speed where the
162 magnitude of resultant aerodynamic force at trailing edge R_n is not too high and upper and lower surface
163 from stagnation point have same length and symmetric shape the flow remains laminar and smooth. As
164 this is a straight body, the fluid particles will have tangents for free-stream at the leading edges and trailing
165 edges of the body and change in θ is very minimal. Thus stream lines formed around the flat plate are
166 nearly parallel to it's surface.So, from Figure 2 it can be stated that for a straight line body which is parallel
167 to the free-stream velocity vector $(\vec{v_\infty})$ there won't be much change in θ_i as long as the velocity is not too
168 high to disrupt the streamlines formed.

169 But as the velocity and length of body increases, we observe that the flow separation and turbulence
170 phenomenon posterior to the trailing edge. Even for a thick plate with considerable frontal area under
171 stagnation, we observe this phenomenon at low speeds. Because at higher velocity of the free stream and
172 large length of body, more energy is lost at stagnation point and subsequent fluid particles gain energy
173 and becomes turbulent as the resultant forces increases continuously and thus flow separation occurs as
174 the magnitude of the force at that particular point of separation is too high $|\vec{F}_i|$ to detach the fluid from
175 streamline. Thus fluid particles detach causing irreversible loss of the flow (turbulence) from the stream
176 line if they have enough energy to deviate from their respective streamlines as shown in Figure 3[3].

177 Similar phenomenon can be observed in flat plates with angle of attack. As more area is opposing the
178 motion of the fluid particles at the area of stagnation is higher and the induced angle of attack contributes
179 to change in the direction of fluid particles as the force is already acting at an angle.[8]Like wise higher
180 velocity of free-stream tends to increase magnitude of resultant force closer to stagnation point. This leads
181 to stall velocity and stalling angle.

182 Based on Reynold's number we can say that the dynamic viscosity (μ) is inversely proportional to
183 the turbulence on the surface of the body[8][5][2].The distance from stagnation point(l), velocity($\vec{v}$) and
184 number of fluids particles available to receive momentum and transfer (ρ) are directly proportional to
turbulence on the body's surface. [9] Therefore, based on historical data we can say that as long as Re<2300
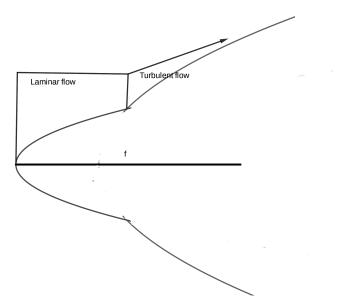
Figure 3. Flow on a flat plate showing boundary layers of laminar and turbulent flows

185
186 at any point on the streamline of the flow will be laminar. Here, l in the equation (6.1) must be understood
187 as the length of stream line rather the length of the body.[9]

$$Re = \frac{\rho v l}{\mu} \begin{cases} Re < 2,300 & laminar\,flow \\ 2,300 < Re < 4,000 & transitional\,flow \\ Re > 4,000 & turbulent\,flow \end{cases} \qquad (22)$$

Based on the conditions specified on can evaluate the nature of flow at any given point on the stream. Here, l should be considered from point of stagnation to the point of consideration on the streamline even if it is posterior to the trailing edge. As it is already well known that the transfer of momentum is a continuum effect in the flow. So, the fluid particles will retain the momentum even after passing away from the body and thus they will tend to flow in turbulent nature posterior to the trailing edge.

Similarly a square or rectangular body will undergo above phenomenon and these can be analyzed using fromulae and assumptions mentioned above. But it will have a larger area subjected to stagnation and which will result in larger magnitude of resultant force $|\vec{F}|$. Thus the fluid particles closer to stagnation point will have higher energy. This will contribute to earlier flow transition and flow separation compared to a flat plate or a streamlined body like an airfoil.

5.2. Flow over a curvilinear body

Consider a body with circular cross-section as shown in Figure 4. It will have a tangents all around the body, unlike flat plate. So fluid particles will have continuous change in θ along their streamline. This is due to the change in the body shape of the body. However as the body is symmetric, the magnitude of the resultant force on the upper surface and magnitude of the resultant force on the lower will be equal i.e. $|\vec{F}_{iu}| = |\vec{F}_{il}|$.[6][8] Similarly, $\theta_{iu} = \theta_{il}$. As discussed in equation (10) and (11), the line integral of angle θ around a curved, symmetric body will be zero. So, under low Reynold's number the flow will not experience any separation and turbulence. However, the change in θ is also continuum depending on the shape of the body[2]. If the change is too significant and sufficient enough for the fluid particles to skip from their stream line with considerable magnitude in the resultant force at a certain point, then flow separation will occur. In this way a symmetric flow separation is occurred when the line of symmetry and free stream vectors are co-linear. This is because the fluid particles will have opposing forces due to the path they traveled and magnitude of the resultant force at the trailing will be high.[6] As fluid particles of same mass and velocity collide which each other they will cause turbulence.
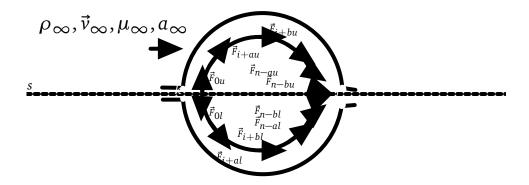
Figure 4. Flow over a circular cross-section body

Now consider a symmetric airfoil which has it's line of symmetric or chord at zero incidence with the free stream. It will not have any vertical force components or simply lift co-efficient is zero($C_L = 0$). But it will have a coefficient of drag or horizontal force component C_{D0}. This is because the vector of resultant force and its direction is in the same direction as the free-stream. Many phenomena like flow separation, stalling, generation of lift and drag can be explained similar to that of flow over a flat plate and curved body.

217 But when the angle of attack is increased, more area is subjected to stagnation compared to flat plate and
218 curved body will have smooth change in θ. Thus symmetric airfoils will have higher performance compared
219 to flat plate at an incidence angle.

220   Flow over an asymmetric body such as cambered airfoils can be explained in the following way. The
221 asymmetric body will have unequal areas on its upper surface and lower causing flow on both surfaces to
222 have different $\vec{F}_i$ and θ_i. Where force on one side is greater than other side and the angle θ on one side of
223 the body is greater than the other side, the resultant forces will be have more magnitude towards one plane
224 even at zero incidence. Thus, camber airfoils will have a lift coefficient ($C_l > 0$) even when $\alpha = 0$. However,
225 they will have an effect called down wash. In cambered airfoils the line integrals of θ on both upper surface
226 and lower surface are not equal. As the length or area of the upper surface is higher than lower surface
227 with higher degree of curvature, It will have θ_u, which is greater than θ_l. Thus stream lines at trailing edge
228 seems little offset with free-stream. However, this effect is negligible, and the angle of down-wash is nearly
229 $\sim 3°to5°$ (based on historical data of aerfoils).

6. Conclusion

231   We enough know that the specified thickness of the body effects by progressively increasing Reynold's
232 number due to more stagnation and energizing the fluid particles.[8] The length of the body will equally
233 contribute by contributing to the change in the magnitude of the resultant force at each consecutive point.[6]
234 These can be expressed using equations given in this article. Curvature of the body effects the streamline
235 by contributing to the change in the angle θ of resultant force at consecutive points from leading edge
236 to the trailing edge. Thus this article mathematically confirms these facts and explains the phenomena
237 such as stalling and effects of camber. With the above mathematical model formation of streamline, flow
238 separation and flow transition can be explained for a given body's shape, size and flow parameters for a two
239 dimensional flow.

240   With FEM this mathematical model can help to estimate flow over a body i.e. to predict the formation
241 of streamline and changes along the streamline with respect to the free-stream velocity, dynamic viscosity
242 and body's shape and size. This model can also be used to reduce the iterations in a design process especially
243 while performing itinerary shaping and sizing of a body in fluid dynamic system or components with open
244 circuit flow. In designing hydrofoils and airfoils, this model can have a significant impact in terms of shaping
245 and sizing compared to conventional methods. In traditional methods of designing streamlined body, where
246 a horizontal tear like body or circle is assumed with arbitrary dimensions (sometimes dimensions based on
247 historical data) and iterated to acquire desired performance. Later, designed models are tested by mostly
248 with scaled models. For a physical scaled model both Reynold's number (Re) and Mach number (M) can't be
249 same as its prototype. Thus, based on flow regime either one of them are not prioritized e.g for high speeds
250 mach number is more important the Re where as for low speeds Re tends to dominate experiment setup.
251 Unlike that, this method can start with a arbitrary dimension at the first preliminary phase and consequently
252 changing the shape at each successive interval or topological surface can deliver a faster design process with
253 less experimentation. In designing a streamlined body the mathematical model presented here presents a
254 lucid and quantitative parameters to design as this formulated model particularly identifies with effects of
255 shape and size of the body. Future scope of work involves developing a CFD(computational fluid dynamic)
256 solver based on the mathematical model prominently mentioned in this article. To objectively evaluate CFD
257 solver and mathematical model using experimental methods.

258   When we implement principles of classical mechanics, the mathematical model is unrealistic and
259 estimated values will have a significant deviation with respect to the real-time phenomenon. Though
260 solid body's shape and size remain constant over the large duration, fluid particles from being static to
261 ionization (under high speeds) will go under various changes that even defies many laws in classical
262 mechanics. Moreover, it is required to extent the current model for a three dimensional flow which can be
263 accommodate not just a laminar flow. A further investigation is required how well this model is applicable
264 for non-Newtonian fluids.

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Nomenclature

α	Angle of incidence	$\vec{F_x}$	Horozontal component of Force
$\Delta\vec{v}$	Change in velocity vector of the fluid particles	$\vec{F_y}$	Vertical component of Force
ΔT	Change in the Temperature	$\vec{F}$	Resultant force due to the fluid motion
μ	Dynamic viscosity of the fluid	$\vec{v}$	Velocity of the fluid
ρ	Denisty of the fluid	A_{ref}	Reference Area
θ	$\vec{F}\angle v_\infty$-angle between the resultant force due to fluid flow and free stream velocity	C_D	Co-efficient of Drag
		C_L	Co-efficient of lift
θ_{r_x}	Angle of resolved force component along X-axis	C_F	Co-effcent of force
		l	length
θ_{r_y}	Angle of resolved force component along Y-axis	A	Effective area
		a	Acceleration of the fluid
θ_{r_z}	Angle of resolved force component along Z-axis	M	Mach number
		m	Mass of the fluid
θ_{rxy}	Angle between two succesive points or space domains along the streamline	Re	Reynold's number
		t	time interval

Subscript

∞	Parameters of free-stream velocity
LE	Leading Edge
TE	Trailing Edge
A_i	Local parameters such as $\rho,\mu,\vec{F}$ and $\vec{v}$ the area (A)
A_{i_q}	Local dynamic pressure on the area (A)
i	Local parameters or derivatives on the streamline
ix	Components of local parameters or derivatives on the streamline in the x-direction or parallel to free-stream
$iu,0u,nu$	Components of local parameters or derivatives on the upper surface of the body
$il,0ul,nl$	Components of local parameters or derivatives on the lower surface of the body
lo	Lower surface of the body
uo	Upper surface of the body
t_1-t_2	Time period between collision and momentum lost
t_2-t_3	Time between fluid particles stagnation and movement

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